# The methanol synthesis

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# Introduction

- Methanol ,also known as methyl alcohol, carbinol, wood alcohol or wood spirit, is a chemical compound with chemical formula <u>CH<sub>3</sub>OH</u>.
- It is the simplest alcohol and is a light, volatile, colorless, flammable and poisonous liquid.
- Methanol is an often used solvent, future alternative fuel and it is also widely used as a raw material for the production of MTBE and other chemicals.
- The demand of this compound is increasing worldwide.

# The methanol, as energy storage material

The output of renewable energy production (wind turbines, photovoltaics) changes significantly with time (exceptions are biogas and geothermal energy), therefore storage capacities are needed to overcome the low production periods in order to ensure the continuous electric energy supply. The feasible solution for energy storage is the use of diverse methods and capacities. George Olah (Nobel prize winner 1994) and his coworkers, in their book about "Methanol Economy" discuss the options and vote for methanol as fuel and

energy storing material.

Methanol can be the alternative of hydrogen!



### **Physical properties**

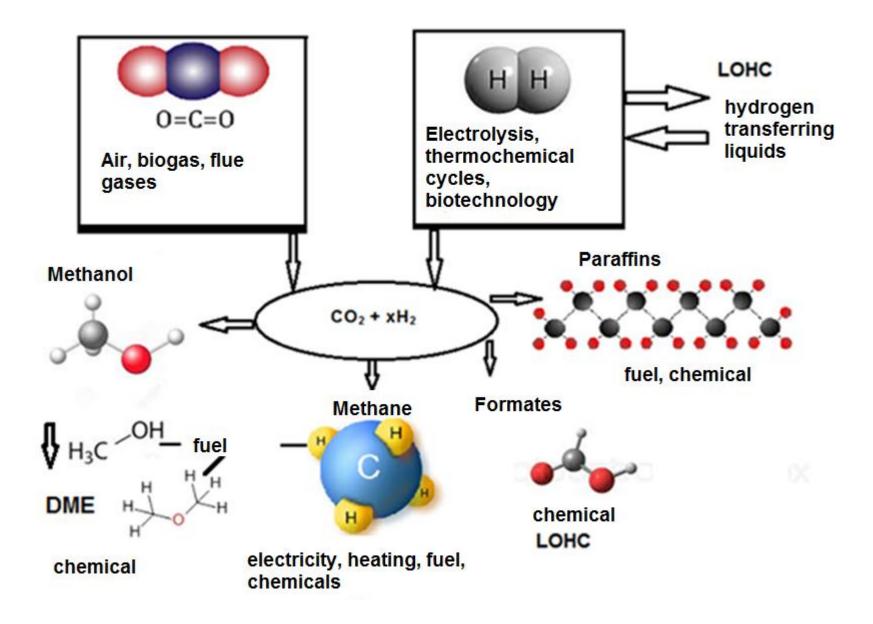
Molecular mass Critical temperature Critical pressure Threepoint temperature Threepoint pressure **Boiling point** Melting point Density Viscosity

Solubility in water

32.4 239.49°C 8.097 MPa -97.56°C 0.10768Pa 64.7°C -97.68°C 0°C 0.8100 g/cm<sup>3</sup> 20°C 0.7913 g/cm<sup>3</sup> 25°C 0.78664 g/cm<sup>3</sup> Liquid 0.5513 mPa s Vapor 9.98× 10 -3

Miscible with water in every ratio

### **Energy storing materials**





## History of the methanol

 Pure methanol, was first obtained in 1661 by Robert Boyle, who called it spirit of box, because he produced it via the distillation of boxwood.

Mittasch and his coworkers prepared a methanol containing mixture from synthesis gas(CO+H<sub>2</sub>) with Fe catalyst in 1913 at BASF. In 1923, the German chemist Matthias Pier, working for BASF also developed a highly selective catalytic reaction to convert synthesis gas (a mixture of carbon monoxide and hydrogen derived from coke and used as the source of hydrogen in synthetic ammonia production) into methanol.

Pressure 25 – 35 MPa Temperatures of about 400°C. Catalyst  $ZnO/Cr_2O_3$  on alumina



In 1966, ICI developed as first a route for methanol synthesis in which sulfur free synthesis gas containing a high proportion of carbon dioxide was reacted on highly selective copper oxide catalysts.

Pressure 5-10 MPa Temperature between 200-300°C

Methanol can now be produced much more economically worldwide by these low pressure methods.

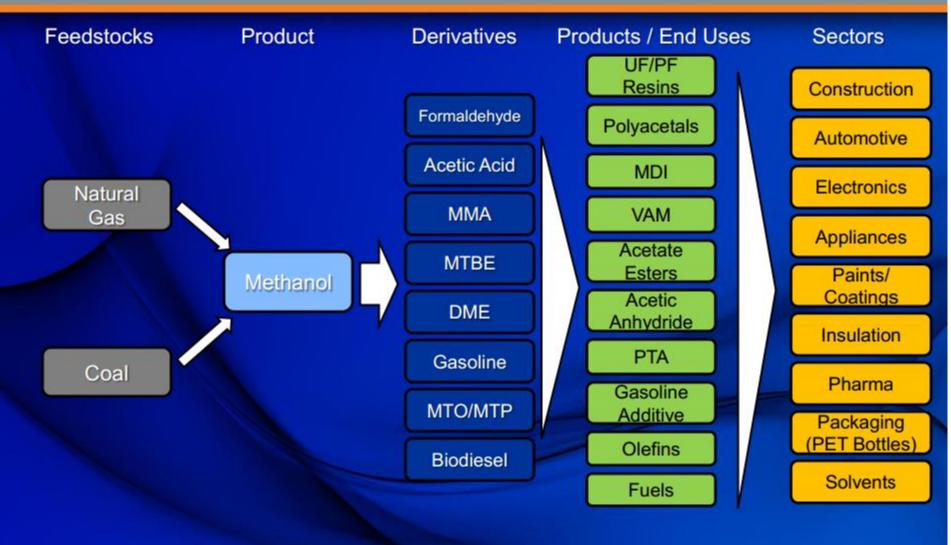


# Uses of the methanol

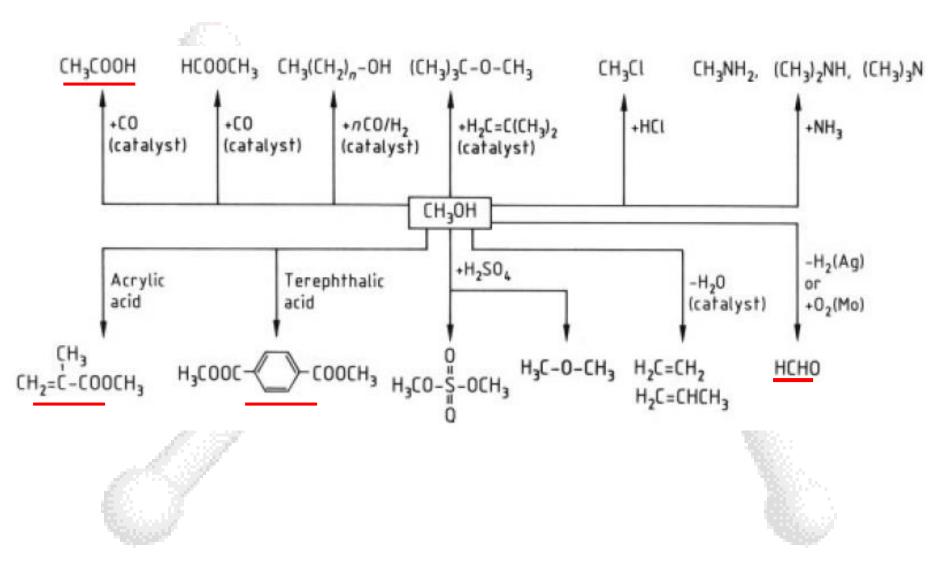
- As a solvent and as an antifreeze in pipelines.
- About 40% of methanol is converted to formaldehyde, and from there into products as diverse as plastics, plywood, paints, explosives and permanent press textiles.
- Large amounts of methanol is used to produce the gasoline additive methyl tert-butyl ether (MTBE).
- Other chemical derivatives of methanol include dimethyl ether, which has replaced chlorofluorocarbons as the propellant in aerosol sprays, and acetic acid.

### **Value Chain - Methanol**





# The use of methanol for synthetic purposes



#### Others 160,000 Methanol-to-Olefins Fuel Cells 140,000 DME Biodiesel 120,000 Gasoline Blending & Combustion Methyl Chloride 100,000 (Chloromethane) Methylamines 80,000 Demand CAGR 14 - 19E = 5.9% Methanethiol (Methyl Mercaptan) Dimethyl terephthalate (DMT) 60,000 Methyl Methacrylate Methyl tert-Butyl Ether (MTBE) 40,000 Acetic Acid



-000- metric tons

20,000

0

2014

2015

2016

2017

2018

2019E

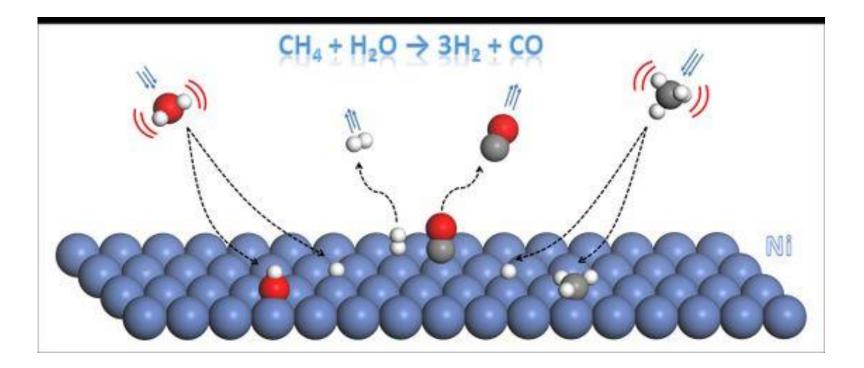


Formaldehyde

# Main parts of methanol production plants

- 1- Purification of raw materials.
  - 2- Reforming.
- 3- Methanol synthesis.
- 4- Methanol purification

Water gas-shift reaction of methane on Ni catalyst





# Methanol Production Processes

Methanol is currently produced on an industrials scale by catalytic conversion of synthesis gas  $H_2$  and CO. The processes are classified according to the pressure used:

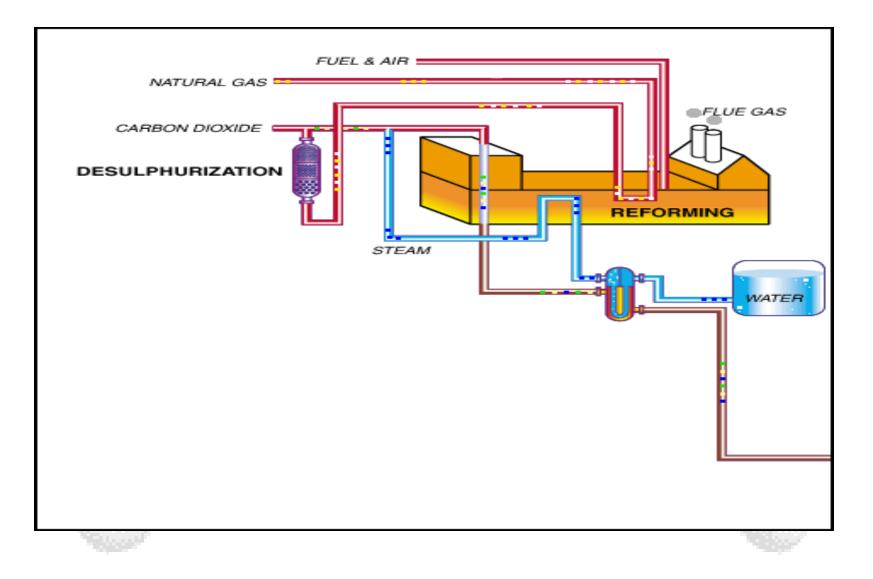
- 1- High pressure process 25-30MPa
- 2- Medium -- pressure process 10-25MPa
- 3- low –pressure process 5-10MPa

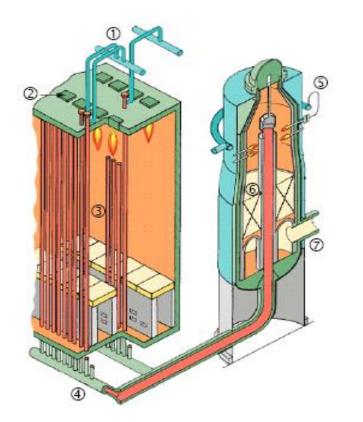
The plants production process that can be divided into four main stages:

- 1- Feed Purification.
- 2- Reforming.
- 3- Methanol Synthesis.
- 4- Methanol Purification.



### Feed Purification and Reforming





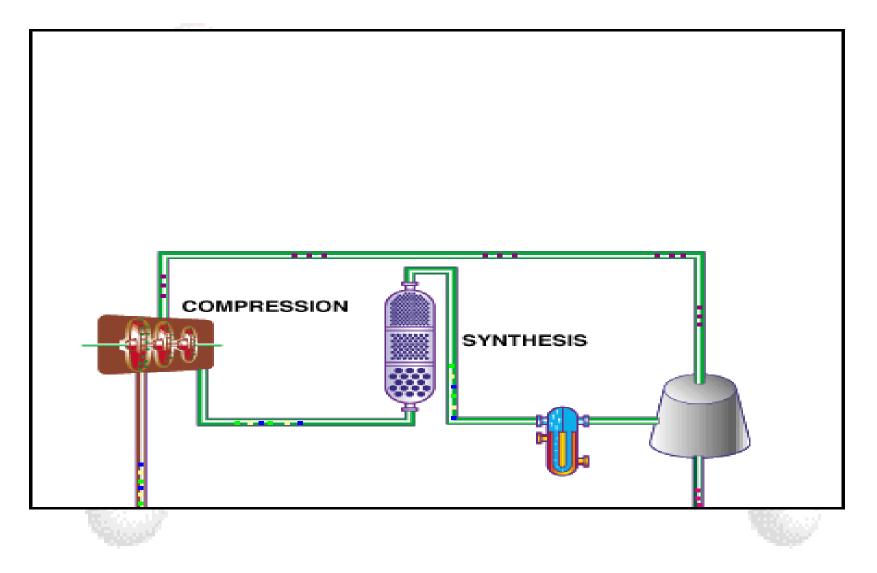
# Uhde radiation and secondary water-gas shift reformer

1) Gas introduction 2) burners, 3) reforming tubes, 4) outlet 5) air introduction, 6) catalyst bed 7) gas outlet

Reforming tubes contain Ni catalyst, pressure 10-20 bar, temperature ~850°C

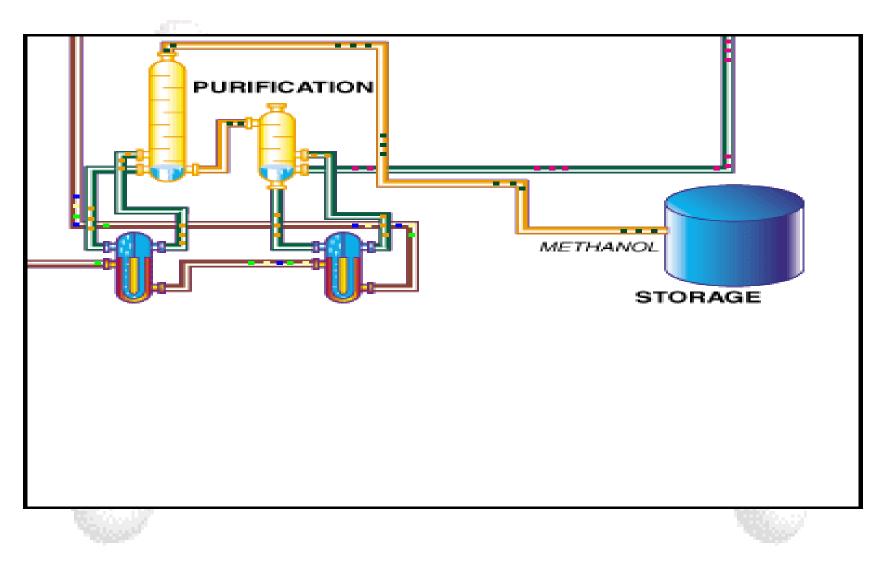








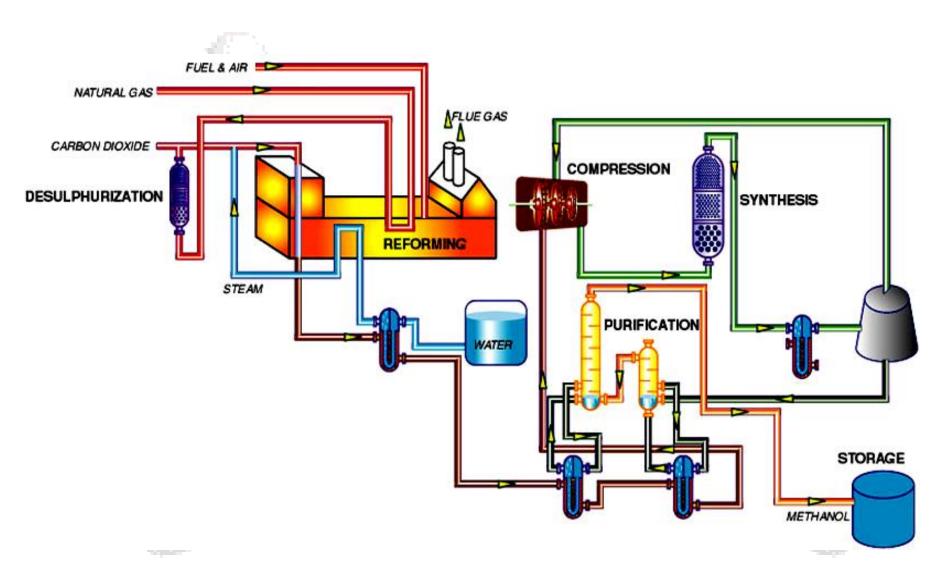






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Methanol Production Processes





## Synthesis Gas Generation

Today, synthesis gas is most commonly produced from methane, from natural gas rather than from coal.

At moderate pressures of 1 to 2 MPa (10–20 atm) and high temperature (around 850 °C), methane reacts with steam on a nickel catalyst to produce synthesis gas according to

 $CH_4 + H_2O = CO + 3H_2$ 

This reaction, commonly called steam-methane reforming or SMR, is endothermic.

The next is the CO conversion:  $CO + H_2O = CO_2 + H_2$ This is exothermic reaction.



# Methanol Synthesis

- There are two main chemical reactions which occur in this process step :
  - $CO + 2H_2 = CH_3OH$  $CO_2 + 3H_2 = CH_3OH + H_2O$
- Production of a crude methanol stream which is about 80% methanol and 20% water, carried out over Cu catalysts.
- Crude methanol is separated from the uncondensed gases and the gases are recirculated back to the converter via the circulating compressor.





### Catalysts for High-Pressure Synthesis

The first industrial production of methanol from synthesis gas by the high pressure process employed a catalyst system consisting of zinc oxide and chromium oxide, which was used at 25-35 MPa and 300-450°C

Catalysts for Low-Pressure Synthesis

All currently used low-pressure catalysts contain copper oxide and zinc oxide with one or more stabilizing additives. Aluminia, chromium oxide or mixed oxides of zinc and aluminum have proved suitable for this purpose. Catalyst Selection



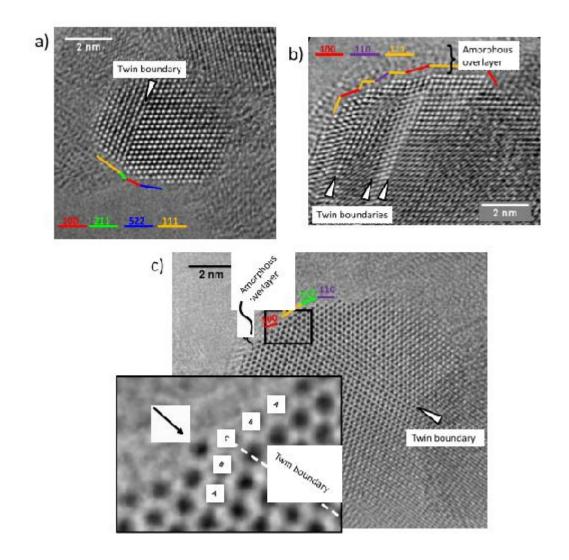
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- Catalyst is an important part in our project especially in reactor because it's fast the reaction.
- Depending on the pressure and temperature of the reactor.

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Catalyst	Definitions	Content	Pressure	Temperature	Poisoned	
	zinc, copper, and chromium		10 MPa	315 °C		
		72 % zinc oxide, 22% chromium(II), 1 % carbon, 0.1 %chromium (VI)	20 Mpa	300 - 400 °C	Low Sulfur, chlorine and phosphorus feed impurities (1924)	
ICI	copper, zinc and Al	copper 60%	Low	270 °C	above 270 oC there is loss of copper surface area	
Titania and zirconia on Cu/Sio2	50 % of Zro2 and 50 % ofTio2 on Cu/Sio2	Cu/Sio2	.65 Mpa	448 - 573 K	methanol synthesis activity seven fold	
zirconia on Cu/Sio3	Zro2 Cu/Sio2	Cu/Sio2	.65 Mpa	448 - 573 K	methanol synthesis activity three- fold	
Titania on Cu/Sio2	Tio2 on Cu/Sio2	Cu/Sio2	.65 Mpa	448 - 573 K	decrease the methanol synthesis activity	
LTS catalyst		Copper		90•C	sulphur and chloride	
KATALCO 83- Series		high copper surface area		250-300°C	High degree of "self- guarding" capacity against trace poisons.	
zinc- chromite catalyst		ZnO-Cr2O3	250 and 350 bar	300 and 400°C	a very high resistance to catalyst poisoning, especially towards sulphur,	
Zinc oxide chromium			20 MPa (200atm)	300 - 400 °C		
cobalt molybdena			500- 700psig	315-430 ℃		

Different types of catalyst for reactor

The industrial catalyst Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> consists of active sites with Cu steps, decorated with Zn atoms and defects which stabilize these steps.



HRTEM pictures about the catalyst surface, with steps, decorating ZnO layer and at the meeting points of regular lattice planes there are the defects.

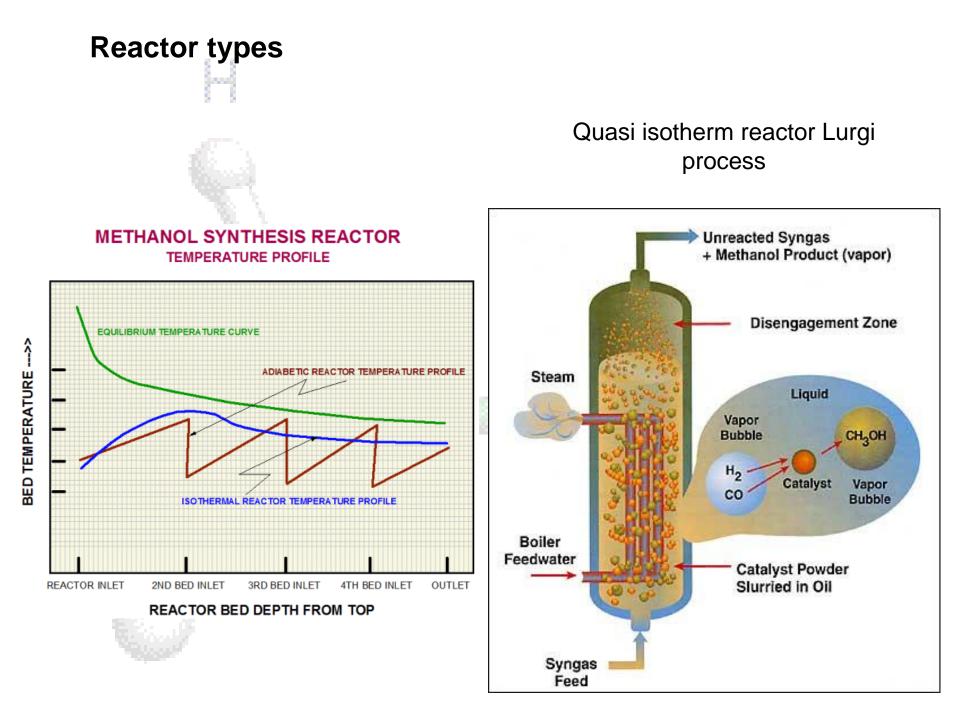


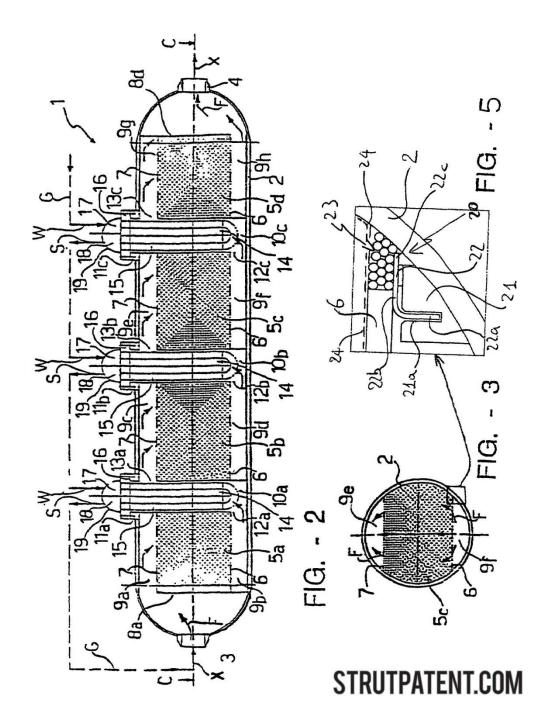
# Type of reactors

Current industrial process for producing methanol differ primarily in reactor design. Many different reactor are available, they may be either adiabatic (e.g.,ICI) or quasi-isothermal (eg., Lurgi). The ICI process accounts for 60%, and the Lurgi process for 30% of worldwide methanol production.

Adiabatic reactor: The ICI process uses an adiabatic reactor.

Quasi-isothermal Reactors. The Lurgi process.

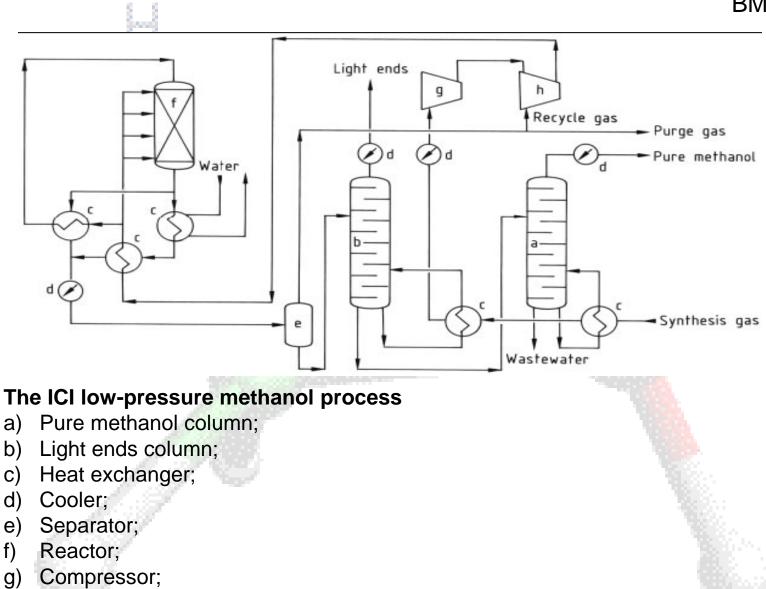




Quasy adiabatic reactor

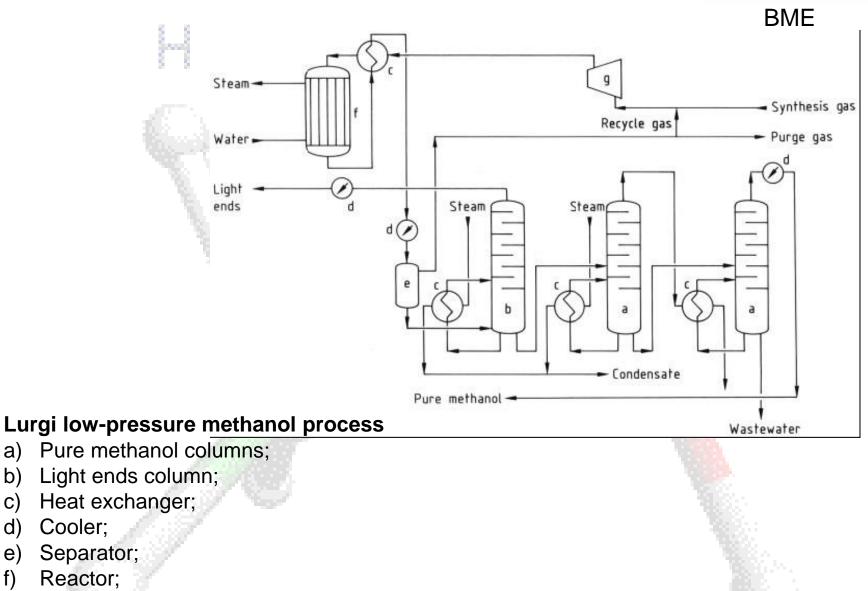
Two solutions: quenching (cold gas feed at intermediate points) Catalyst bed sections with cooling in between





h) Compressor recycle stage





Compressor recycle stage g)

a)

b)

C) d)

e)

f)

# New possibilities of methanol synthesis

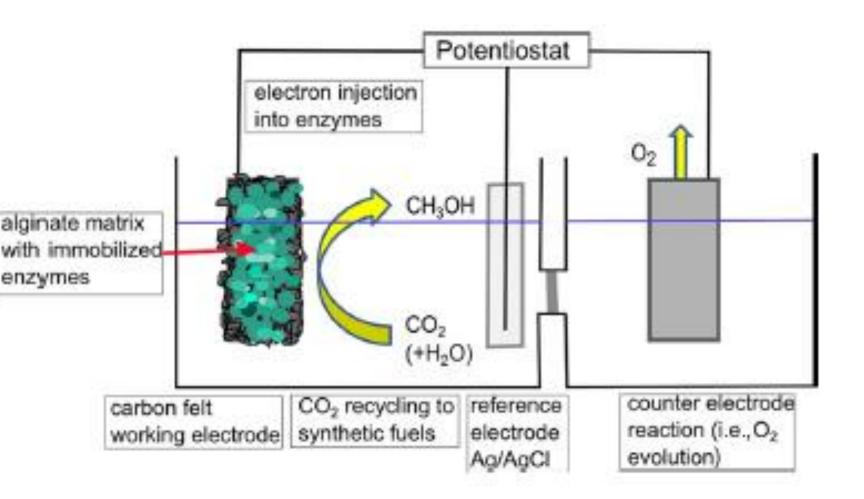
The conversion of  $CO_2$  to methanol with **homogeneous catalytic reactions with Ru complexes**, among mild conditions (40 bar, 80°C) with promising reaction rates.

Electrochemical reduction, with low selectivity and effectiveness

Anodic reaction	$2H_2O \rightarrow O_2 + 4H^+ + 4e^-$ ; $E_0 = 1.23$ V vs. NHE				
Catodic reaction	$CO_2 + 6H^+ + 6e^- \rightarrow CH_3OH + H_2O; E_0 = 0.02 \text{ V vs. NHE}$				

Combination of electrochemical and photochemical catalytic methods is promising!

Figure 1. Representation of the electrochemical CO<sub>2</sub> reduction using enzymes. Electrons are injected directly into the enzymes, which are immobilized in an alginate-silicate hybrid gel (green) on a carbon-felt working electrode. CO<sub>2</sub> is reduced at the working electrode. Oxidation reactions take place at the counter electrode.





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## Storage and transportation

#### Storage

- In totally enclosed equipments, tanks
- Avoid ignition and human contact
- Tanks must be grounded and vented and should have vapor emission controls.
- Avoid storage with incompatible materials.



#### Material Selection for storage tank

Anhydrous methanol is non-corrosive except:

Lead

- Magnesium
- Methanol is non-corrosive except:
  - lead
  - Aluminum
- Mild steel is the recommended construction material.





Biodegradation / Aquatic Toxicity:

- Methanol biodegrades easily in
  - Water.
  - Soil.

Methanol in high concentrations (>1%) in fresh or salt water can have short-term harmful effects on aquatic life within the immediate spill area.



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# Thank you for your attention!

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